

M/ 39148-US

= DE-C-1248943

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90,379P	VII-B, X-GI.	20.7.65. BADI
DISCONTINUOUS DEODORISATION OF AQS. POLYMER DISPERSIONS.		
GE. 1.248,943 clg. (Non-Con)	20.7.65. (GE) as B 82,909	Pub. 31.8.67. Badische Anilin.
<p><b>NEW</b> Volatile impurities are removed from aqs. polymer dispersions by passing steam into boiling dispersion taking resultant foam-steam mixt. and separating</p> <p><b>ADVANTAGES</b> Simple discontinuous method requiring no costly plant. Economic use of steam. Effective deodorisation.</p> <p><b>USES</b> Esp. in conjunction with batch polymerisation.</p> <p><b>SPECIFICALLY</b> Dispersions pref. have surface tension &lt;40 dyne/cm. and may be aqs. dispersions of (co)polymers from vinyl chloride, vinyl esters, (meth)acrylic esters, styrene, butadiene, polymers con-</p>	<p>taining SO<sub>2</sub>H and/or COOH and/or CONH<sub>2</sub> groups or dispersions containing sulph(on)ated emulsifiers. Volatiles include excess monomer, low-mol. by-products, emulsifiers and other auxiliaries. Foam-steam mixt. is broken at flow rates &gt;100 m/sec. by rapidly diminishing pressure by ~100 - 350 torr. &lt;0.2%, often &lt;0.1% volatiles remain.</p> <p><b>EXAMPLE</b> 800 kg. 50% aqs. dispersion of 50% n-butyl acrylate/50% styrene copolymer were heated to 62°C in 1 m<sup>3</sup> vessel, which was evacuated to 30 torr. so that contents boiled. Foam and steam formed were pushed up rising tube, passed through constricted nozzle-like end, where foam was broken, and into separator. Broken foam was recycled. 130 kg/hr. steam were injected through bottom of</p> <p>Cont'd.....</p>	
<p>vessel, keeping contents at 69°C. Pressure loss in rising tube and nozzle was &gt; 180 torr. After 3 hr., residual monomer content had fallen from 1.65 to 0.018% (based on solids in dispersion).</p>		
	D16/AKA/KA/MAS	90,379P